

A new raw material in the production of biodiesel: purple pinion seeds.

Uma nova matéria-prima na produção de biodiesel: sementes do pinhão-roxo.

Aluísio Marques da Fonseca^I; Margareta do Carmo^{II}; Regilany Paulo Colares^{III};
Camila Peixoto do Valle^{IV}; Sara Jane de Oliveira^V; Juan Carlos Alvarado Alcócer^{VI};
Olienaide Ribeiro de Oliveira Pinto^{VII}; José Cleiton Sousa dos Santos^{VIII};
Emerson Yvay Almeida de Sousa^{IX}; Francisco Felipe Maia da Silva^X

Abstract

Biodiesel is an alternative fuel that is produced through oil plants or animal fat. It is a renewable energy source, with biodegradable characteristics, to emit less pollutant than diesel. Thus, this work aims to show the production of biodiesel from the purple-pinion (*Jatropha gossypifolia* L.) seeds. In addition to the synthesis, the physical-chemical characterization of both the raw material and the final product was carried out. The biodiesel synthetic route was performed by the basic catalytic transesterification reaction, using potassium hydroxide (KOH) in the presence of methanol (CH₃OH) in the molar ratio of 1: 3 (oil: methanol). As a result, it was observed that the mass conversion of the biodiesel was 22.05 g. The physical-chemical analyzes carried out were acid index of 0.106 mgKOH / g, according to ANP technical resolution. The peroxide index of 1.03 meqO₂ / kg, the kinematic viscosity of 20 ° C to 40 ° C, obtained was 6.455 mm²/s and 3.5343 mm²/s, the values are close to the ANP technique resolutions. Stability was 0.26 hours, and the biodiesel burning test was executed for approximately 3 hours. Therefore, there is a high viability of biodiesel production through the purple pinion seeds.

Keywords: Renewable energy; Transesterification; *Jatropha gossypifolia* L.; Physical-chemical characterization.

Resumo

O biodiesel é uma alternativa de combustível que é produzido através das plantas oleaginosas ou gordura animal. É fonte de energia renovável, com características biodegradáveis, por emitir menos poluentes que o diesel. Assim, este trabalho tem como objetivo mostrar a produção de biodiesel a partir das sementes pinhão-roxo (*Jatropha gossypifolia* L.). Além da síntese, foi realizada a caracterização físico-química, tanto da matéria prima, como o produto final. A rota sintética do biodiesel foi realizada pela reação de transesterificação via catalise básica, utilizando o hidróxido de potássio (KOH) na presença de metanol (CH₃OH) na razão molar de 1:3 (óleo: metanol). Como resultado, observou-se que a conversão em massa do biodiesel foi 22,05 g. As análises físico-químicas realizadas foram: índice acidez de 0,106 mgKOH/g, estão de acordo com resolução técnica da ANP. O índice peróxido de 1,03 meqO₂/Kg, a viscosidade cinemática de 20°C a 40°C, obtida foi de 6,455 mm²/s e 3,5343 mm²/s, os valores estão próximos das resoluções de técnica da ANP, a estabilidade oxidativa foi 0,26 horas, e o teste de queima do biodiesel durou aproximadamente 3 horas. Portanto, existe uma alta viabilidade de produção do biodiesel através das sementes de pinhão roxo.

Palavras-chave: Energia renovável. Transesterificação. *Jatropha gossypifolia* L. Caracterização físico-química.

^I Doutor, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. aluisiomf@unilab.edu.br

^{II} Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. lawanukhey@gmail.com

^{III} Doutor, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. regilany@unilab.edu.br

^{IV} Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. camilapeixotovale@unilab.edu.br

^V Mestranda, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. saraqumica@hotmail.com

^{VI} Doutor, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. jcalcocer@unilab.edu.br

^{VII} Doutor, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. agron.olienaide@gmail.com

^{VIII} PHD, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. jcs@unilab.edu.br

^{IX} Mestre, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. emersonquimicoufc@hotmail.com

^X Doutor, Professor, Universidade da Integração Internacional da Lusofonia Afro-Brasileira, CE, Brasil. felipe.maia@ifrn.edu.br

1 Introduction

The search for alternative fuels has been gaining prominence in recent decades. The fossil fuels substitution is motivated by environmental, economic and social factors, since the whole society depends on its use. In this sense, one option highlighted is to use biofuels (OLIVEIRA et al., 2008).

The biofuels utilization becomes a viable solution for the fuel demands to replace fossil fuels. Among the most interesting alternatives are the sources of biomass considered adequate and available for the consolidation of renewable energy programs. The use of plant biomass can be a solution to reduce the costs of fuels, such as electric power generation, turning them more accessible to isolated populations that depend on non-renewable energy sources (SILVA FILHO, 2010).

Thus, the definition of biofuel could be: any useful product for the energy generation, obtained totally or partially of biomass (TOLMAS-QUIM, 2003). During thousands of years biomass was an important primary energy source for the planet. Several organic sources can be used as biomass for the development of various society sectors, among them biofuel from oleaginous plants.

Vegetable oil is one of the largest sources of biodiesel. Biodiesel is a fuel produced from vegetable oils or animal fats and an alcohol (methanol or ethanol), in the presence of an acidic or basic catalyst, a process called transesterification (FERRARI, 2005).

To manufacture biodiesel can be used oil plants such as soybean, castor bean, jatropha, purple pineapple, babassu, rape seed, canola, palm, cotton, sunflower, saffron, coconut, peanut, canola, crambe, etc.; therefore, from the use of organic material to produce biodiesel it is possible to bring innumerable benefits to the environment, in addition to social aspects, comparing to fossil fuels (KNOTHE et al., 2006). In this way, biodiesel assumes a prominent role, presenting economic, social and environmental advantages, adding value to the studied biomass as it presents as a byproduct, few pollutants and to release less CO and CO₂, besides being recycled in the agriculture, through agriculture family.

Present work aims to show the biodiesel production from purple pinion (*Jatropha gossypifolia* L.) seeds, applying the basic catalytic via transesterification methodology adopted by Knothe et al. (2006) with some adaptations.

2 Material and Methods

2.1 Search Location

The Seeds of Purple Pinion were collected in the municipality at “Redenção” at the geographical coordinates latitude (S) 4° 13 ‘33” and longitude (WGr) 38° 43’ 50” northeast at “Baturité” Massif, in the “Ceará” state (IPCE, 2017).

The research was carried out in the Organic Chemistry laboratory, University of International Integration of

African-Brazilian Lusophony (UNILAB) at the Auroras Campus, and in the fuels laboratory at “Ceará” Industrial Technology Nucleus (NUTEC).

The methodology for the preparation of biodiesel had the following steps: after the collection, the seeds were dried for oil extraction. Then, the characterization was carried out by the transesterification reaction (alcohol + KOH) and decantation (glycerol + water). At the end of the process, esters were used for the acid wash were obtaining the biodiesel.

The reagents and solvents used in the synthesis and characterization of the products were all analytical grade, from the DYNAMIC brand. The reagents and solvents used were: hexane P.A (C₆H₁₄); Sodium Hydroxide (NaOH); Potassium Hydroxide (KOH); Diatomite Phenolphthalein (C₂₀H₁₄O₄); Methanol P.A (CH₃OH); Hydrochloric Acid (HCl); Potassium Iodide (KI); Soluble Starch (C₆H₁₀O₅)_n; Sodium Thiosulphate (Na₂S₂O₃); Acetic Acid (CH₃CO₂H); Chloroform (CHCl₃); Sodium Chloride (NaCl); Distilled water (H₂O) and Anhydrous Sodium Sulfate P.A (Na₂SO₄).

2.2 Purple Pinion Seeds Separation Parameters

The Purple Pinion’s seeds were collected in the Redenção municipality in pasture area. The seeds were dehydrated in a greenhouse for a period of three (3) days at 75 °C.

This process was done to improve the quality of the seeds and promote the homogenization in the extraction of oil from the purple pinion. Before drying in the greenhouse, the seeds with shells were weighed. Then, the seeds were separated between the shells and the capsulated seeds. In the separations of both, the seed mass was obtained in grams (g), and soon after were crushed in a blender.

2.3 Processes to obtain oil from the seeds of purple pinion

The extraction was made with a cold non polar organic solvent (Hexane P.A) in a closed container, then left for a period of three days at room temperature between the range of 24 °C to 30 °C. After the three days, the liquid was separated by filtration. Then, the solvent/oil mixture sent to the rotary evaporator under the reduced pressure, which after dry with anhydrous sodium sulfate, the fixed oil was obtained (crude). In this final step, crude oil passed into a refining process.

To calculate oil production rate, equation 1 was used:

$$\text{Yield (\%)} = \frac{\text{Extracted oil Mass}}{\text{Seed Mass}} \times 100 \quad (1)$$

2.4 Refined Oil Obtainment

Aiming the raw material’s quality improving at biodiesel production, the fixed oil obtained by extraction with organic solvent was subjected to a refining process, called neutralization followed by bleaching. The methodologies were adopted by Morais et al. (2001); Days (2009); Rodrigues (2013) and Moretto and Fett (1998).

The process for the refining oil used the following steps: The crude oil underwent a neutralization process, then filtration and bleaching, result being the refined purple pine nut oil.

2.4.1 Neutralization

Crude oil was neutralized according to the methodology (DAMODARAN, PARKIN; FENNEMA, 2010). To perform the neutralization, the values of the acidity index and the crude oil's mass should be known, where it was added to a predetermined amount of sodium hydroxide (NaOH) at 20%. The mixtures were stirred at 250 rpm to 60 °C, in a period of approximately 45 minutes. After 45 minutes, the sample was subjected to the absence of temperature and kept under magnetic agitation until reaching the ambient temperature, the mixture was left at rest for 3 hours.

2.4.2 Whitening

To neutralized oil was added 1% of Diatomite, then heated for 30 minutes the temperature of 70 °C, under magnetic agitation. After 30 minutes, the heating was switched off and the magnetic agitation remained until the sample reached room temperature. The sample remained at rest at room temperature for 5 hours, where it was filtered in filter paper for 24 hours. After that, the refined oil was collected for the biodiesel production. This step was adapted from the methodology (MORAIS et al. 2001).

2.5 Analysis after treatment and characterizations: raw material's oil and biodiesel

The Raw Material (purple pinion oil) was characterized for the acidity index, peroxide index, oxidization stability, specific mass and kinematic viscosity. For biodiesel, the analyzed characteristics are density, kinematic viscosity of 20 °C to 40 °C, oxidative stability, fluidity, acidity index and peroxide index.

2.5.1 Acidity Determination

2g of purple pinion oil was weighed in a 125 mL erlenmeyer flask. Added 25 mL of neutral ether-Alcohol (2:1). It was added two drops of Phenolphthalein and was titrated NaOH 0.1 M until the appearance of a pinkish coloration, which should persist for 30 seconds. The same procedure was performed with biodiesel, with the methodology adapted by the INSTITUTO ADOLFO LUZT (2008) and acidity values were based on the standard EN 14104. The calculation is made by the expression in milligrams per KOH per gram of oil mgKOH/g, determined by Equation 2:

$$I. A = \frac{V_g \times f \times M \times 5.61}{P_A} \quad (1)$$

Where, A. I is the acidity index, Vg represents the volume spent on sodium hydroxide titration of 0.1 M, F is the correction factor of the NaOH solution 0, 1M, M is the molarity of the alkaline solution and P_A Is the mass of the sample in grams (g).

Another possibility of determining the acidity index is the expression through the percentages of free fatty acids (FFA %). Thus, it is important to know the average of the molar weights of free fatty acids present in the oil, that is, to know the molar weight of oleic acid. Then use the equation 3:

$$F. F. A\% = \frac{V_g \times f \times M \times 28.2}{P_A} \quad (3)$$

That can be summarized as in Equation 4:

$$F. F. A\% = 0.503 \times I. A \quad (4)$$

2.5.2 Peroxide Index determination

The oil was weighed between the range of 5 ± 0.05 g of the sample in a 250 mL Erlenmeyer flask. It was added 30 mL of the acetic acid/chloroform 3:2 solution and stirred until the dissolution of the sample. Shortly thereafter, 0.5 mL of a saturated KI solution was added, where it left at rest under the light for approximately one minute. It was Added 30 mL of distilled water and was titrated with a sodium thiosulphate solution of 0, 01N, with constant agitation. The Titration continued until the yellow coloration disappeared. It was Added 0.5 mL of indicator starch solution and continued titration until the disappearance of the blue color. The same process Was made for biodiesel, with the Methodology adapted from the INSTITUTO ADOLFO LUZT (2008).

The determination of the peroxide index was made by the expression milliequivalents per 100g of sample (meq/100), and the calculation was determined by the equation 5:

$$P. I. = \frac{(V_1 - V_2) \times N \times f \times 1000}{P_A} \quad (5)$$

Where, P.I is the Peroxide index, V₁ represents the titration expenses of sodium thiosulphate 0.01 N solution in the sample in mL, V₂ represents the blank titration expenses, F is a factor of sodium thiosulphate solution and P_A is the number of gram (g) of the sample.

2.5.3 Oxidization Stability; Determination of the specific mass and kinematic viscosity

To stabilize the purple pinion oil's oxidation, and biodiesel, is utilized standard EN 12112, adopted in Brazil by the ANP. The equipment used in the tests was the Rancimat from METROHM®.

The specific mass or density and viscosities of the oils of purple pinion and biodiesel were from 20 °C to 40 °C, the samples were based according to the standards NBR 14065 and ASTM D445.

2.5.4 Fluidity Determination

The fluidity point is an important method for biodiesel in which the temperature of the liquid cannot drain freely. It happens because biodiesel varies in every second depending on the origin of the raw material. So, these properties are considered important for ambient temperature where the fuel should be stored and used.

For the determination of the fluidity point, the ASTM D-97 method was used in the apparatus CPP5Gs.

2.6 Processes of obtaining biodiesel from purple pinion

In the production of biodiesel, there are several methods for its synthesis. However, this work was planned to do the transesterification process via basic catalysis. Next are all the steps for the transesterification process, a methodology adapted by (KNOTHE et al., 2006).

2.6.1 Potassium methoxide preparation

It was weighed approximately 0.62 g of KOH and dissolved in 10.5 mL of CH_3OH , the 45 °C. The resulting solution was used in the next step.

2.6.2 Purple pinion oil transesterification

Added 8.52 g of purple pinion's refined oil, in a Becker, warmed up in a sand bath at 45 °C, for 5 Minutes. Therefore, the solution of potassium methoxide, under agitation, was left to the heated oil, reacting for 30 minutes to 45 °C under magnetic agitation. Transferred the mixture to a separation funnel, waiting long enough for the separation of the phases (approximately 15 minutes). He Collected the upper phase, containing the biodiesel.

2.6.3 Neutralization and the biodiesel obtained washing

It was added 15 mL of 0.5% HCl in the mixture, the phase separation was stirred. It was collected the aqueous solution and repeated this procedure with 15 mL of a saturated NaCl solution. Finally, after separating the NaCl solution, added distilled water at 45 °C, stirred, waited for the separation of the phases and collected distilled water and measured the pH until to neutral 7.

2.6.4 Combustion Test

Three beckers were numbered and to each of it was added a cotton swab moistened with methanol, refined oil of purple pinion and biodiesel. It was set fire and observed.

2.7 Test for cholinesterase inhibition quantification

The inhibitory activity of the enzyme acetylcholinesterase (AChE) was measured in plates of 96 wells of flat

fungus using Elisa BIOTEK Reader, model ELX 800, software "Gen5 V 2.04.11", based on the methodology described by Ellman et al. (1961). In 96 wells Plates, the following solutions were used per pit: 25 μL of Acetylthiocholine iodide (15 mM), 125 μL of 5.5'-Ditiobis-[2-nitrobenzoic] in the Tris/HCl solution (50nM, pH = 8, with 0.1 M of NaCl and 0.02 M of $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$. (3 mM, DTNB or Ellman reagent), 50 μL of the Tris/HCl solution (50 nM, pH = 8, with 0.1% of bovine serum albumin (BSA)), 25 μL of the Extract sample dissolved in Ethyl Acetate and diluted 10 times in the Tris/HCl solution (50 mM, pH = 8) To obtain a final concentration of 0.2 $\text{mg} \cdot \text{mL}^{-1}$ (TREVISAN et al., 2003).

The absorbance was measured at 405 nm for 30 seconds. Then, 25 μL of the acetylcholinesterase enzyme were added (0.25 $\text{U} \cdot \text{mL}^{-1}$) and the absorbance was measured per minute up to a total of 25 minutes of incubation of the enzyme. As a negative standard, all solutions were used, except for the sample.

The dilutions of the samples and of the positive patterns used in the quantitative assessments in Microplate, departed from a mother solution with a concentration of 20 mg/mL were: 200, $\mu\text{G} \cdot \text{mL}^{-1}$, 100 $\mu\text{G} \cdot \text{mL}^{-1}$, 50 $\mu\text{G} \cdot \text{mL}^{-1}$, 25 $\mu\text{G} \cdot \text{mL}^{-1}$, 12.5 $\mu\text{G} \cdot \text{mL}^{-1}$, 6.25 $\mu\text{G} \cdot \text{mL}^{-1}$, 3.12 $\mu\text{G} \cdot \text{mL}^{-1}$, 1.56 $\mu\text{G} \cdot \text{mL}^{-1}$, and 0.78 $\mu\text{G} \cdot \text{mL}^{-1}$.

The values referring to the natural colorations of the extracts were excluded from the analysis. The percentage of acetylcholinesterase inhibition was calculated by comparing the reaction velocities (substrate hydrolysis) of the samples in relation to the white (considered total activity of AChE, 100%). The pattern used as positive control is physostigmine.

All samples were analyzed in triplicate, as follows. The samples had their own coloration absorbed by the reading wave spectrum, thus, the values referring to the staining were deducted. After the data normalization, a non-linear regression curve test was performed using the GraphPad Prism v 5.01 Statistical program.

2.8 Composition of the diesel oil obtained from the purple pinion-Mass Spectrum (MS)

Diesel oil analysis was performed in GC/MS Shimadzu/QP2010 using a capillary column RTX-5 (30 m x 0.25 mm, 0.25 μm film thickness) and the drag gas is helium. For the temperature analysis for the essential oil furnace was programmed of 40-180 °C at a rate of 4 °C/min, after 180-280 °C at a rate of 20 °C/min and maintained at 280 °C for 10 min. For the fixed temperature analysis of the oil furnace was programmed of 80-280 °C At a rate of 5 °C/min, then from 280-300 °C at a rate of 20 °C/min and kept at 300 °C for 5 min. The Kovat retention indexes were calculated using a series of standard N-alkane (C7-C30). The identification of the compounds was performed by comparing their mass spectra with those of the NIST08 library, retention indexes and published data (ADAMS, 2007).

3 Results and Discussion

For the determination of pinion purple's seeds separation parameter, it was obtained a moist seeds mass with shells in the value of 2 kg, while the mass reached from shelled seeds was 888.58 g.

In Table 1, it is showed the results of the cold extraction with Hexane P. A of the purple pinion seeds. The extraction process occurred for three days and were conducted during 5 stages. It was Observed that during the extraction of the oil showed different yields.

There are several methods for the vegetable oil extractions that leads to a large percentage viability (MORRETO; FETT, 1998), However, the best-known processes are the pressing and extraction by organic solvents That are used both for the extraction biomass oils of animal origin (fats) as vegetable (oilseed plants). In the data obtained with the extraction of oils from the seeds of purple pinion, it was considered that the methodology used expressed results Satisfactory, in which a total of Mass (g) of Crude Oil of *Jatropha gossypifolia* (COJG) equal to 92.28 g and rate 10.38%, as shown in Table 1.

Table 1 - Purple Pinion seeds cold extraction results with hexane P.A.

Extractions	COJG Mass (g)	Rate in %	Time in hours
I	30.0	3.37	72
II	20.5	2.30	72
III	17.8	2.00	72
IV	15.9	1.79	72
V	8.08	0.91	72
Total	92.28	10.38	

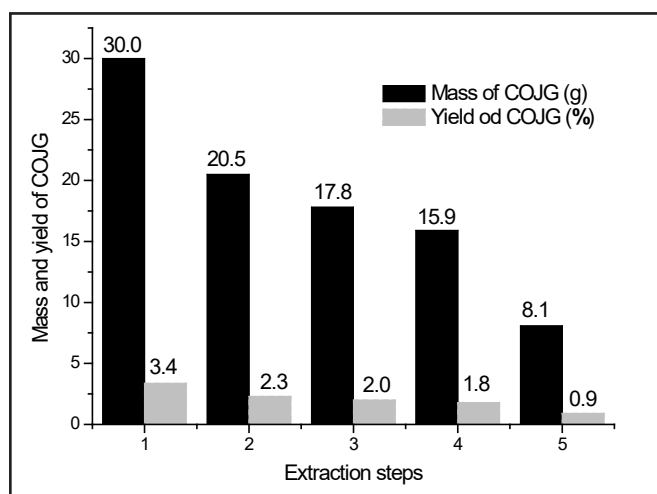
Source: Authors (2019)

According to the Reis e Silva researchers (2011), were carried out extraction of purple pinion seed by Soxhlet using hexane P. A as organic solvent, presenting a rate of 7.17%, with the seed mass 37.77 g being the oil mass 2.93 g. Comparing with the results obtained with the purple pinion seeds collected in the municipality of "Redenção" in which the rate was 10.38%, and crude oil mass 92.28 g. Is possible to report that both methods, for plant oil extraction *Jatropha gossypifolia* was feasible in oil extraction. However, the data obtained in this study were higher than the data achieved by Reis e Silva (2011).

Figure 1 shows the variations of crude oil masses and the rate for purple pinion. The seeds mass from unpeeled purple pinion was 888.58 g. It was extracted with hexane solvent P.A. The extraction was done five times. According to Silva (2010), the Plants of the Family Euphorbiaceae feature maximum extraction rate ranging between 9.09% and 33%. So, the extraction process with the purple pinion seeds was quite satisfactory. A variation rate and the oil mass obtained were constant.

For a good quality in biodiesel production it must have occurred the alkyl ester and glycerol separation, so that the oil extracted from the purple pinion's seeds received a treatment, which was the clarification or bleaching of the oil. Lipids are macromolecules that

Figure 1 - Crude oil mass variation in extraction steps



Source: Authors (2019)

present a class of chemical substances whose main characteristic is the non-polarity and solubility in organic solvents (MARTINS; LOPES; ANDRADE, 2013). So, should be withdrawn the impurities of soaps residues, traces of heavy metals, oxidization products, phosphate residues and material unsaponifiable (PAIVA, 2010), this can prevent the separation process, which is arduous, to break the long chains of triglyceride.

Therefore, this step of the refining process to remove the undesirable impurities mainly the pigments, was added an adsorbent celite diatomite type of land activated to crude oil, in which the Heating and The Filtration. celite diatomite is a type of clarifier adsorbent, the bleaching process of this work was also added the sodium hydroxide 20% in relation to the amount of acidity of the raw material, this method for the neutralization of oil. The adsorbent selectively removed the pigments that are β carotene (yellow and red $C_{55}H_{56}$), Xanthfila (Yellow $C_{40}H_{56}O_2$), and chlorophyll (blue $C_{55}H_{72}O_5N_4Mg$ and Yellow $C_{55}H_{70}O_6N_4MG$). The comparisons between them were made in oil whitening visualization, where dark crude oil spent for yellow light oil. This was satisfactory for biodiesel production.

Refined oil of *Jatropha gossypifolia* (ROJG) obtained presented mass of 46.09 g with a 49.95% rate in total crude oil mass. The refined were 20 g for the characterization of the raw material and the rest 26.09 g were for the process of obtaining biodiesel.

In Table 2, is presented the values of physical chemic characterization of oil pinion-purple and determination of acidity Index and peroxides index.

According to Silva (2010) oil with high acidity may compromise the motor life, because it presents a corrosive action in metal parts, which can affect the engine operation. Acidity Index determination as a chemistry parameter to determine the quality of vegetable or fat's oil can provide an important data in its preservation. Therefore, it is important to know the amount of oleic acid in general, for to set the quantity in milligrams of potassium hydroxide to neutralize a sample gram.

Comparing the values obtained with the oil's physical

Table 2- Characterization of the seeds of purple pinion.

Parameter	Unity	COJG	ROJG	STANDARD
IA	mgKOH/g oil	4.61	0.47	Adolf Lutz
AGL	%	231.9	23.64	-
IP	meqO ₂ /Kg oil	3.52	2.05	Adolf Lutz
Specific Mass at 20 °C	g/cm ³	0.9114 ± 0.001*	-	NBR 14065
Specific Mass at 40 °C	g/cm ³	0.8976 ± 0.001*	-	NBR 14065
Kinematic Viscosity at 20 °C	mm ² /s	45.312 ± 0.01*	-	ASTM D445
Kinematic Viscosity at 40 °C	mm ² /s	21.965 ± 0.01*	-	ASTM D445
Oxidative Stability	hours	3.73± 0.38*	-	EN 14112

Source: Authors (2019)

chemical characterization for the purple pinion with crude oil, refined oil and biodiesel, it was found that the crude oil value obtained was 4.1 mg KOH/g reducing to 0.47 mg KOH/g refined purple pinion oil. If raw material's acidity is high, then it is found low conversion efficiency. The excess and insufficient catalyst can cause the formations of soaps. Thus, the product obtained from biodiesel was 0.106 mg KOH/g which is within the standard.

Peroxide determination is a relevant parameter for fuel production quality. According to Knothe et al. (2006), the Oxidation of an unsaturated fatty acid begins with the accumulation of peroxides. However, the oxidation of oils or fats as a high catalytic value can slow down or reduce by influence of the free radical. The consequences caused are temperature variation, enzymes, light and metal ions.

The biodiesel mass stability limit is illustrated in Table 2. The specific mass used must be in accordance with NBR 14065 Standard. However, the values obtained with the purple pinion seeds at different temperature present a variation between 20 °C to 40 °C where was obtained 0.9114 g/cm³ and 0.8976 g/cm³. The Importance of this characteristic with the viscosity is that it exerts a great influence in process such as injection fuel and the preparation for automatic ignition.

The values of kinematic viscosities of the purple pinion oil in temperatures varying from 20 °C to 40 °C presented values between 45.312 mm²/s and 21.965 mm²/s The Ratio of the obtained values is satisfactory

and feasible to produce biodiesel.

Oxidative stability is one of the analyses of great importance for the oil profile of the raw material, because appropriated values allow its use In motor consumption, as it can promote stability or durability operation of the machine. The Value obtained In oil test shows that the biodiesel product will be stable in decomposition caused by an air flow. The Induction time is determined by the conductivity measurement. The evaluation is completely automatic.

The molar ratio between alcohols (methanol): Purple pinion oil was 1:3 in temperature 4°C for 30 minutes. Reaction occurred completely and the separation of phases occurred in 15 minutes. According to Knothe et al. (2006), the process of transesterification via basic catalysis of refined vegetable oils in molar ratios of alcohol (methanol): Oil of at least 6:1 in temperature ≥ 60°C, the reaction can be completed at 1 hour.

After obtaining Biodiesel, one drop was in the burn test. The burning time was 3 hours. Crude and refined oils do not burn during the given time. Therefore, it is possible to affirm that durability in the use of combustion motors will be viable. Besides may be exist possibility of another consumption form as its utilization at kerosene stove.

Table 3 presents the results of the characteristic analyzes of biodiesel of *Jatropha gossypifolia*. L. In the determination of the acidity of the biodiesel of *Jatropha gossypifolia*. L, it is observed a value 0.106 mgKOH/g

Table 3 - Purple pinion biodiesel characterization

Parameter	Unity	Value	Methodology
IA	mgKOH/g oil	0.106	Adolf Lutz
AGL	%	5.33	-
IP	meqO ₂ /g oil	1.03	Adolf Lutz
Kinematic Viscosity to 20°C	mm ² /s	6.455	ASTMD-2270
Kinematic Viscosity to 40°C	mm ² /s	3.5343	ASTMD-2270
*Density to 20°C	g/cm ³	0.8812	NBR14065
*Oxidation Stability	hours	0.26	EN14112
*Fluidity	°C	-3	ASTMD-97

Source: Authors (2019)

being compatible and satisfactory with the technical resolution number 1/2008 of ANP that set the maximum biodiesel acid standard in 0.5 mgKOH/g. The interference to the reduction of acidity posed by a treatment of the seeds of purple pinion, where the high value interferes in the transesterification reaction.

This means that most of the free fatty acids present in the oil participated in the transesterification reaction and produced the methyl esters. For these reasons, the monitoring of the acidity in biodiesel is of great importance during the storage, since it changes its values for a period, this means that the presence of the water favors the reactions of hydrolysis and proliferation of microorganism, favoring the degradation.

The biodiesel peroxide purple pinion index is 1.03 meqO₂/Kg of oil, however in technical resolution number 2/2016 by ANP there's no limit value specified. This parameter is very important because it carry the degradation information about compose material in oil and in the biodiesel. According to Malacrida and Jorge (2006) the high limit doesn't must be above 10 meqO₂/g.

The kinematic viscosity between 20 °C to 40 °C is 6.455 mm²/s and 3.5343 mm²/s. The standard from ANP is 3 mm²/s for 20 °C and 6 mm²/s at 40 °C. Its values are in agreement with the N° 1/2008 ANP resolution. The values presented in this work are inside the limits allowed by Brazilian legislation. The biodiesel kinematic must be less than viscosity for purple pinion oil. The relations for kinematic viscosity are showed in Tables 2 and 3.

Comparison between the two values of the raw material and the conversion showed a reduction in the relation between the density and the kinematic viscosity. The density of purple-pinion biodiesel was 0.8812 g / cm³, compared to the limit value of technical resolution ANP No 7/2008 is 850- 900 kg / cm³. The value obtained from

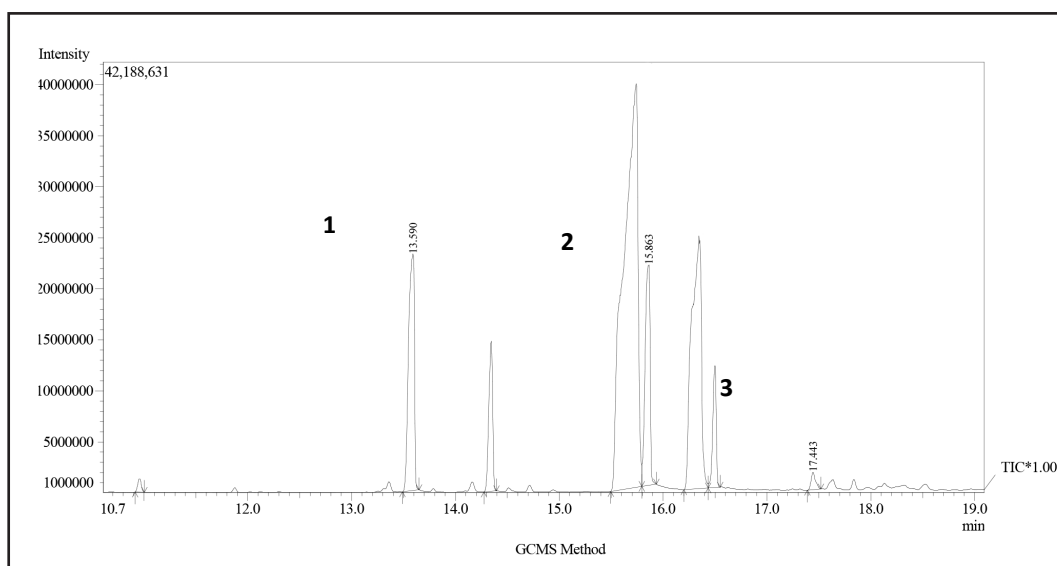
the density is within the standard. This parameter is important for proper operation of the vehicle injection system, which is dependent on the raw material. Excess alcohol lowers density.

Oxidative stability determines the degradation of biodiesel. However, the value of the test for the stability of the purple pinion biodiesel was 0.26 hours; this test was based on the European standard (EN14112) by the Rancimat method. In relation to the Rancimat method, several studies show that the induction time determined results in the degradation quality of biodiesel as acidity index and kinematic viscosity. The oxidative stability of the purple-pinned methyl biodiesel was low and the induction time did not reach the limit value for ANP biofuel, this may be the greater presence of linoleic acid (C18: 2), which gives it the lowest oxidative stability (MELO, 2008).

The fluidity test is one of the specific properties of biodiesel, where it is possible to verify the ignition problem at start and performance in the fuel system of the vehicle subject to low temperatures. The tendency of the fuel is to solidify or freeze. The melt flow value was -3 °C for purple-pinion oil. The reduction occurs because the spatial composition of saturated fatty acids organized in the hydrocarbon chains aid in freezing. Therefore, this value possibly of the purple pinion methyl biodiesel presented the interaction of hydrogen bonds with the participation of oleic acid. In relation to ANP standards, there is no limit to these parameters until now.

After determining the esterification reaction by basic catalysis and using methanol as an acetylating agent by GC / EM, the formation was verified on a chromatogram providing a mixture of three peaks, which characterized as the main constituents of this oil. The results are shown in Figure 2.

Figure 2 - Purple pinion biodiesel chromatogram showing the characteristics formation peaks. (1) Dodecanoic acid, (2) tridecanoic acid and (3) 8-octadecinoic acid.



Source: Authors (2019)

Table 4 - Purple pinion biodiesel composition by chemical route

Peak#	R. Time	Name	Base m/z	Area%
1	13.590	Dodecanoic acid methyl ester	74.05	54.01
2	15.863	Tridecanoic acid methyl ester	74.05	42.93
3	17.443	8-octadecinoic acid methyl ester	55.05	3.06

Source: Authors (2019)

Table 5 - Normalization curve for non linear regression by statistic software GraphPad Prism v5.01

Samples	IC ₅₀	Std. Error	R ²
Standard	1.15	0.05	0.99
Purple Pinion Ext. EtOH	12.46	0.06	0.85

Source: Authors (2019)

As shown in Table 4, the major components found in the fixed oil of purple pinion were the acids: dodecanoic, tridecanoic and 8-octadecinoic.

Table 5 shows the normalization of the non-linear regression curve. In the IC₅₀ means values were performed the variance test with multiple comparison between pairs by the Tukey test, being considered significant values of P < 0.05.

4 Conclusion

The purple pinion seeds extracted with organic solvent of hexane P. A, have a 10.38% rate, being considered good. The treatment of the oil obtained features a 49.95% rate and conversion into methyl esters of 118.32%.

The choice of basic catalytic transesterification allows the acidity index of the purple pinion oil crude to be 4.61 mgKOH/g, being higher than the refined oil that is 0.47 mgKOH/g and from biodiesel, which is 0.106 mgKOH/g. All these numbers are into the ANP standard given by resolution no 1/2008.

The values of the characteristics between the crude oil, refined, and its conversion to methyl esters reduces, in spite of the process of treatment of the purple pinion oil in the significant form, therefore, the final production rate in oil is very necessary, since there was a significant improvement in the parameters analyzed and also facilitates the production of biodiesel.

The parameters found for biodiesel, even if not compliant with some minimum specifications of the national ANP standard but show that the biodiesel produced through the purple pinion seeds has potential for use as biofuel.

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